

LH₂-Absorber Development

Daniel M. Kaplan
Illinois Institute of Technology

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Outline:

1. New absorber dimensions
2. Energy absorption
3. Absorber cooling design approaches
 - a. external cooling loop
 - b. absorber as heat exchanger
4. Window requirements
5. Other options
6. Prototype & test plans

LH₂ Absorbers

Typical absorber specifications:

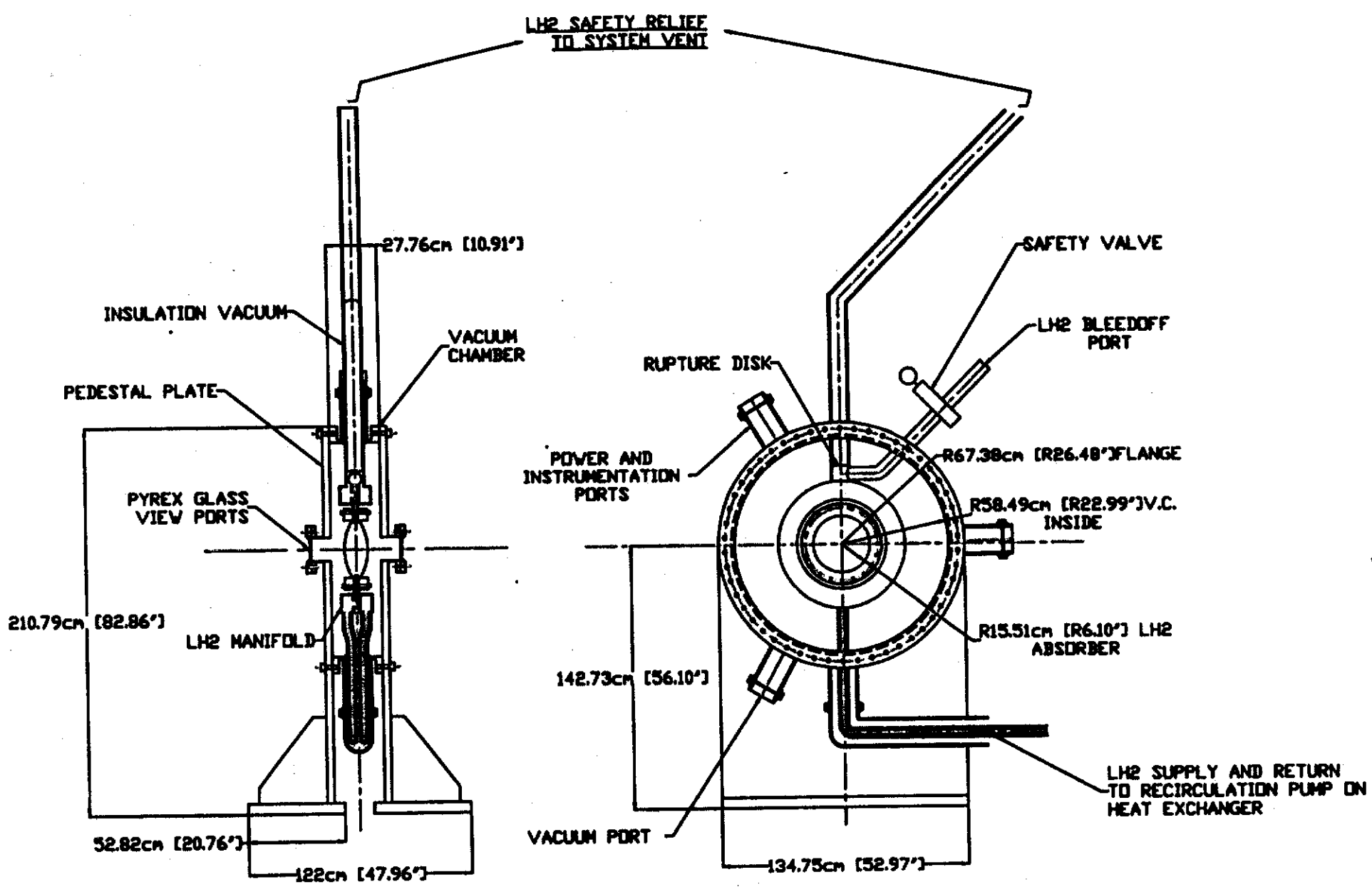
Config. Param.	Single-Flip	FOFO1	FOFO2	unit
<i>L</i>	30	12.6	13.2	cm
ρ	0.0708	0.0708	0.0708	g/cm ³
<i>areal mass density</i>	2.1	0.89	0.93	g/cm ²
<i>r</i>	20	15	10	cm
<i>V</i>	38	9	4	l
<i>T</i>	20	20	20	K
<i>P</i>	2	2	2	atm
<i>b.p.</i>	22.8	22.8	22.8	K
<i>f.p.</i>	13.8	13.8	13.8	K

Energy absorption vs. muon momentum:

<i>p_μ</i>	$\langle dE/dx \rangle$	$\langle \Delta E \rangle$	$\langle P \rangle (5.10^{12} @ 15\text{Hz})$
(MeV/c)	[MeV/(g/cm ²)]	(MeV)	(W)
106	6.0	13	230
211	4.2	5.6	160
317	4.1	5.5	157
106	6.0	3.4	97
211	4.2	2.4	68
317	4.1	2.3	66

} 30 cm

} 12.6 cm



SIDE SECTIONAL VIEW

FRONT VIEW
(FRONT PEDESTAL PLATE REMOVED)

TEST STAND FOR THE FOFO ABSORBER

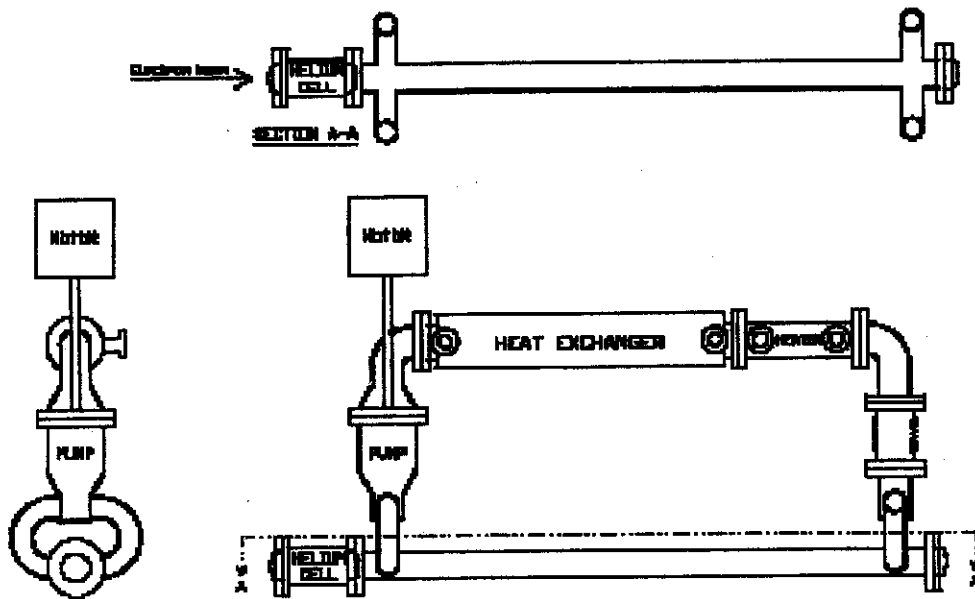
E. Black
IIT/FNAL
5/8/2000

Key Problem:

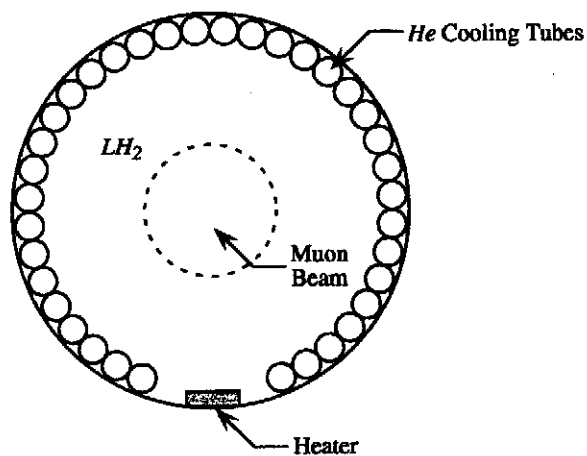
- How to get the heat out?

→ Two design approaches:

1. External cooling loop



2. Absorber as heat exchanger



LH₂ Cooling

1. External-loop design (à la SLAC, Bates...):

$$c_p = 1.1 \times 10^4 \text{ J/kg} \cdot \text{K}$$

$$\Delta T / s = \frac{\langle P \rangle}{c_p V \rho}$$

$$\leq \frac{180 \text{ W}}{1.1 \times 10^4 \text{ J/kg} \cdot \text{K} \times 38 \text{ l} \times 0.0708 \text{ kg/l}} = 0.006 \text{ K/s}$$

30-cm case ←

→ Indep. of L since both $\langle P \rangle$, $V \propto L$

⇒ need < 0.05 volume change/s

= 1.9 l/s (Single-Flip)

(4x less for FOFO1)

→ should be no problem

LH₂ Cooling (cont'd)

2. Convection approach (K. Cassel, IIT):

Rate of heat transfer from LH₂ to He coolant:

$$\dot{q} = - \frac{A(T_o - T_i)}{\left(\frac{1}{h_{LH_2}} + \frac{\Delta x}{k_w} + \frac{1}{h_{He}} \right) \ln \left(\frac{T_{LH_2} - T_o}{T_{LH_2} - T_i} \right)}$$

where

- A = surface area of cooling tubes
- T_i = temp. of helium in
- T_o = temp. of helium out
- T_{LH_2} = avg. temp. of LH₂
- h_{LH_2} = convective heat transfer coeff. for LH₂
- h_{He} = convective heat transfer coeff. for He
- Δx = thickness of cooling-tube walls
- k_w = thermal conductivity of cooling-tube walls

Example (30-cm case, guesstimate $h_{LH_2} \approx 130 \text{ W/m}^2 \cdot \text{K}$):

$$\dot{q} = - \frac{0.25 \text{ m}^2 (15\text{K} - 14\text{K})}{\left(\frac{1}{130 \text{ W/m}^2 \cdot \text{K}} + \frac{1 \text{ mm}}{170 \text{ W/mK}} + \frac{1}{1580 \text{ W/m}^2 \cdot \text{K}} \right) \ln \left(\frac{20 - 15}{20 - 14} \right)}$$

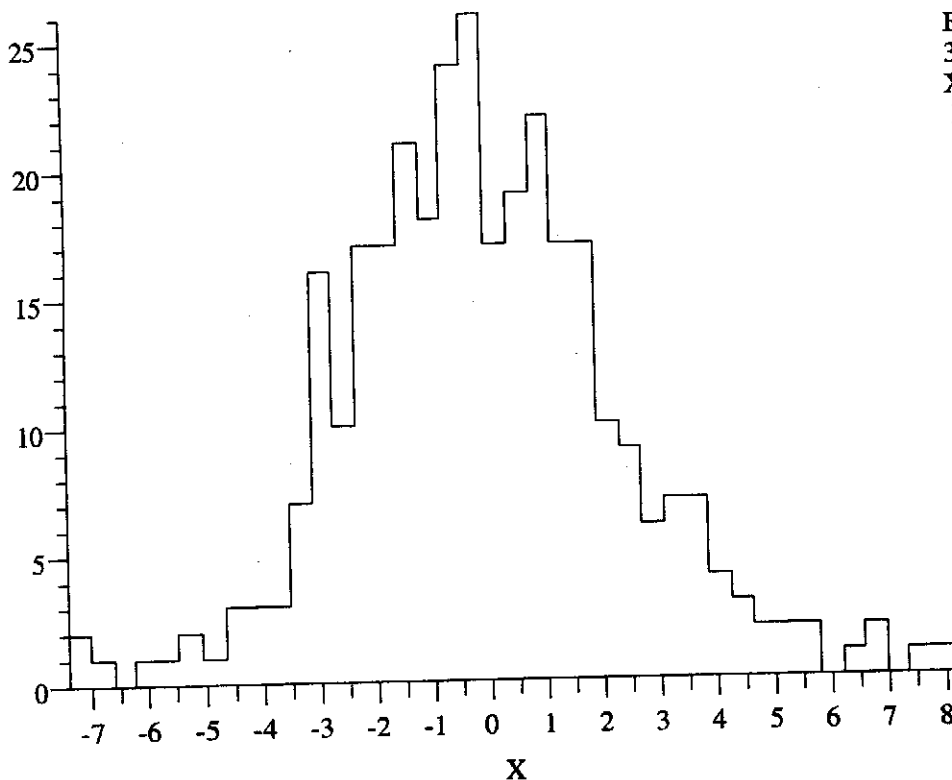
$$= 180 \text{ W} @ \dot{m} = 0.0248 \text{ kg/s} \Rightarrow \dot{m}/\rho = 3.5 \text{ l/s} @ 2 \text{ atm, } 14 \text{ K}$$

BUT - need to understand $h_{LH_2} \Rightarrow \text{CFD}$

Spatial distribution of heat load:

- **Energy deposition highly concentrated in the middle!**
 - By end of cooling channel, areal power density along axis is $\sim 10^2 \times$ average over face of absorber
 - ⇒ need to ensure cross-flow near beam rather than longitudinal flow
 - occurs naturally in convective design
 - also possible in external-loop design,
- Parametrize spatial distribution by $s \equiv \sigma_x / r \gtrsim 0.25$:

X (Beam at Low beta (Zl=0) at Section 40)



CFD Study of Fluid Flow:

(K. Cassel & M. Boghosian, IIT)

- What matters in convective design is h_{LH_2}
→ depends on \dot{q} in a manner to be determined by computational fluid dynamics (CFD):

On a 2D grid, iteratively solve Navier-Stokes and energy equations to calculate Nusselt number vs. Rayleigh number, where

$$Ra_D = \frac{g\beta D^5}{\nu\alpha K} \frac{\dot{q}}{V},$$

$$Nu_D = \frac{D}{K} h_{LH_2},$$

and

$$g = 9.8 \text{ m/s}^2$$

$\beta = (1/V) dV/dT =$ volumetric coeff. of thermal expansion

$D =$ diameter of absorber

$\nu =$ kinematic viscosity of LH_2

$\alpha =$ thermal diffusivity of LH_2

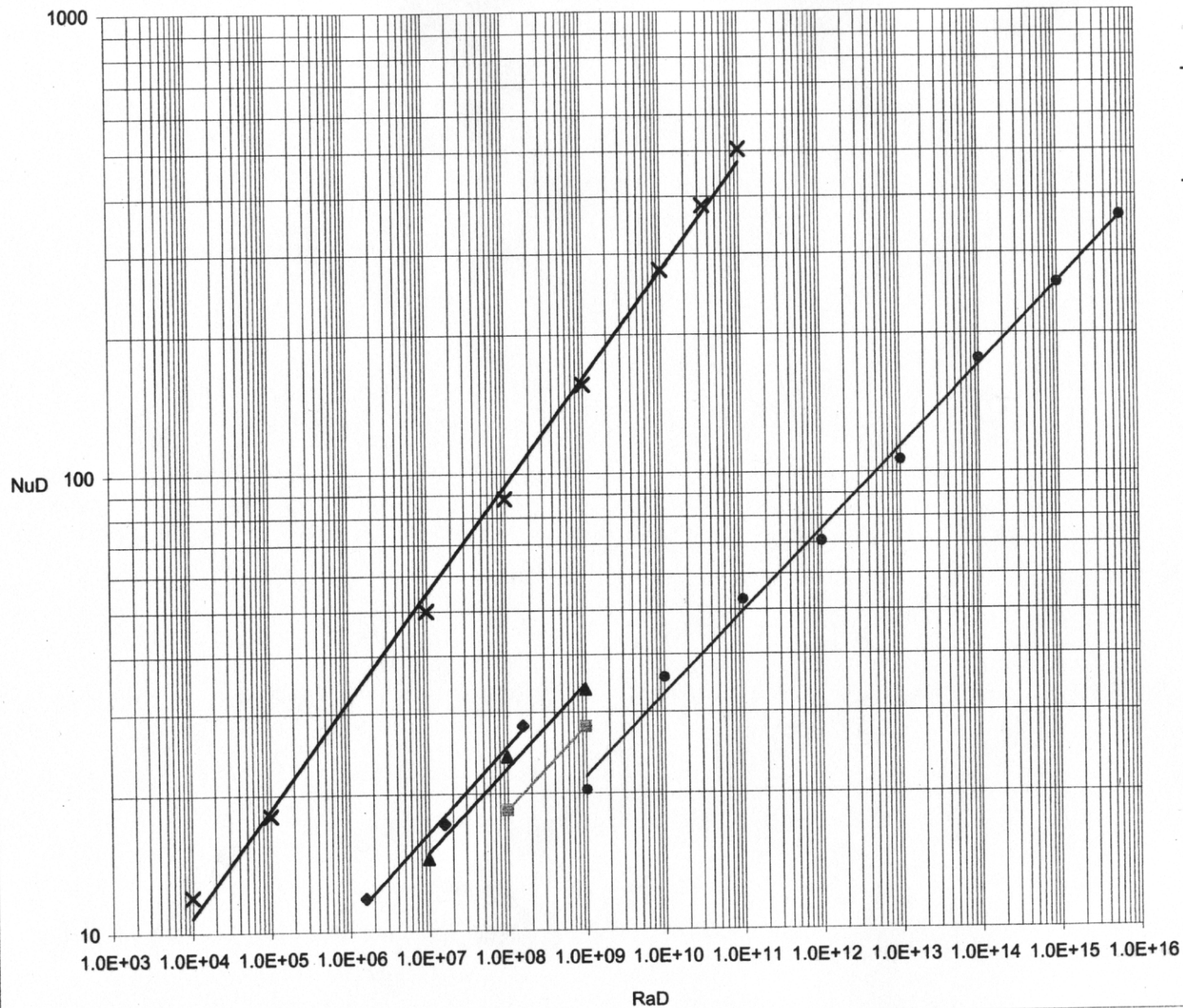
$K =$ thermal conductivity of LH_2

$V =$ volume of absorber

- Given $K = 0.0987 \text{ W/m}\cdot\text{K}$, $D = 0.4 \text{ m}$,
need $Nu_D \approx 400$ to give $h_{LH_2} \approx 130 \text{ W/m}^2\cdot\text{K}$

$$\Rightarrow Ra_D \sim 10^{15} \text{ for } s = \sigma_x/r \approx 0.25$$

Correlation of the Average Nusselt Number vs. Rayleigh Number
(Horizontal Cylinder with Internal Heat Generation)



Window Thickness

- ASME UG-32, head thickness for pressure vessels:

hemispherical: $t = \frac{0.5PL}{SE - 0.1P}, \quad s = L = 0.5D$

ellipsoidal: $t = \frac{0.5PD}{SE - 0.1P}, \quad s = 0.25D$

torispherical: $t = \frac{0.885PD}{SE - 0.1P}, \quad s = 0.169D$

where P = pressure differential
 L = radius of curvature
 D = length of major axis
 S = max allowable stress
 E = weld efficiency
 s = sagitta

Notes: 1. ellipsoid has (major axis) = $2 \times$ (minor axis)
 2. "torisphere" has $r_2 = 6\% r_1$

- Fermilab/ASME safety factors:

S = smaller of $S_u/4, S_y/1.5$

- 6-month study:

Take $E \approx 0.9$ (inspected full-penetration welds), Al alloy,
 1 atm:

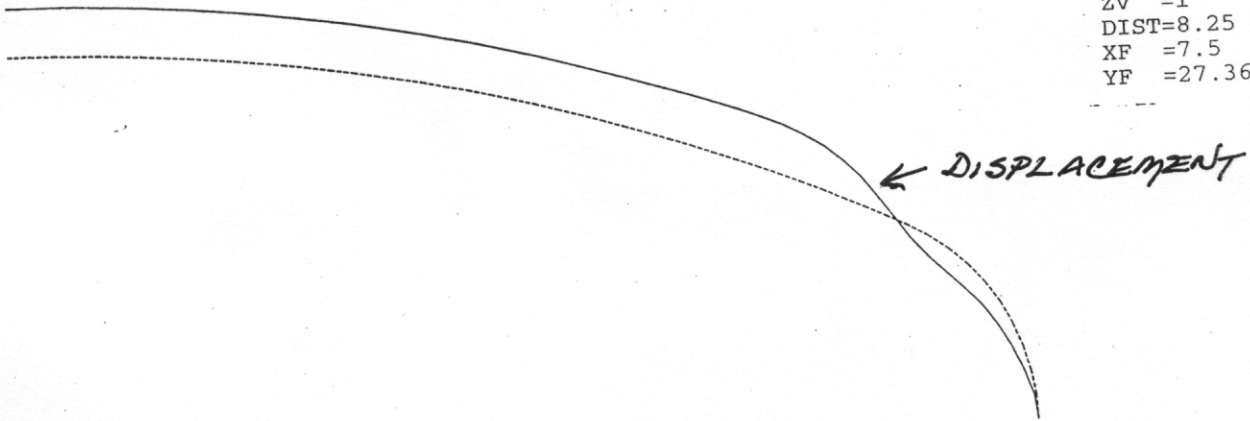
Case:	Single-Flip	FOFO1	FOFO2
Parameters:	$r = 20$ cm, ellipsoidal	$r = 15$ cm, torispherical	$r = 10$ cm, ellipsoidal
Thickness:	300 μm	400 μm	200 μm

TORISPHERICAL FEA STUDY

ANSYS 5.5.1SP
MAY 4 2000
09:34:40
PLOT NO. 2
DISPLACEMENT
STEP=1
SUB =1
TIME=1
PowerGraphics
EFACET=1
AVRES=Mat
DMX =.029918

DSCA=25.068
ZV =1
DIST=8.25
XF =7.5
YF =27.361

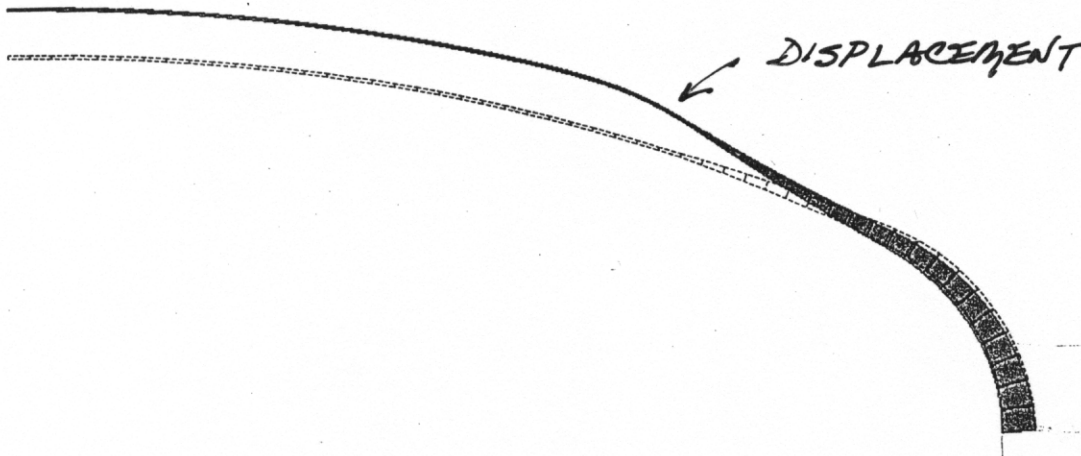
UNIFORM



ANSYS 5.5.1SP
MAY 4 2000
13:27:05
PLOT NO. 2
DISPLACEMENT
STEP=1
SUB =1
TIME=1
PowerGraphics
EFACET=1
AVRES=Mat
DMX =.009677

DSCA=78.794
ZV =1
DIST=8.387
XF =7.625
YF =27.379
Z-BUFFER

"TAPERED"



Recent window progress:

1. Safety may preclude operation at ≈ 1 atm:

- J. Kilmer (Fermilab): risk of cryopumping air contamination into vent lines

→ recommends 2 atm

⇒ might R&D on safety design allow operation as low as 1.1 atm?

2. ASME standard assumes uniform thickness

- ANSYS FEA calculation (Z. Tang, Fermilab):

→ can be $\approx 30\%$ thinner in middle if suitably thicker at edges

- Integral flange (machined, not welded) $\Rightarrow E = 1$

- Will continue to iterate → try to reduce thickness further

Case:	Single-Flip		FOFO1		FOFO2	
Params:	r = 20 cm, 1 atm, ellipsoidal, E = 0.9	r = 20 cm, 1.1 atm, improved torispherical,* E = 1	r = 15 cm, 1 atm, torispherical, E = 0.9	r = 15 cm, 1.1 atm, improved torispherical, E = 1	r = 10 cm, 1 atm, ellipsoidal, E = 0.9	r = 10 cm, 1.1 atm, improved torispherical,* E = 1
Thick:	300 μ m	367 μ m	400 μ m	275 μ m	150 μ m	180 μ m

*Note: torispherical shape \Rightarrow improved circulation near windows

Other Ideas:

1. Thinner windows

AlBeMet? Beryllium? (compatible with LH₂?)

	ρ	S_y	S_u	X_0
Material	(g/cm ³)	(MN/m ²)	(MN/m ²)	(cm)
Al (6061-T6)	2.7	241	289	8.9
AlBeMet	2.1	314	413	18.8

2. LiH?

Hazardous to handle since reacts with H₂O, releasing hydrogen and igniting!

Not available commercially in large pieces

On our list of things to think about...

3. "No" windows!

Use high-pressure (≈ 20 atm) cold gaseous hydrogen
 \Rightarrow 1 thick window at each end

- OK if $\beta \approx$ constant (e.g. single-flip, DFOFO)
- \rightarrow would need R&D on operating RF cavities in high-pressure hydrogen atmosphere (freon/SF₆ admixture?)

Prototype Test Plans

(M. A. C. Cummings, NIU)

1. Destructive Al window test at $\geq 4P_w$
2. (Cryogenic) material tests of AlBeMet
3. Fluid-flow bench tests (certify CFD calcs)
 - LH₂ analogue (water?) at room temp.
 - heat fluid electrically?
 - monitor heat transfer in each heat-exchanger tube?
 - understand signatures of boiling
4. Cryo bench test
5. High-power beam test

Beam Tests

• Requirements:

1. Availability within next \approx year
2. Particle energy and flux sufficient to penetrate absorber and deposit $\sim 10\text{W/cm}$
3. Accommodate one or more LH_2 absorbers and possible solenoid
4. Desirable: near Fermilab

• Options:

Argonne: (poor solution – low flux or poor equipment access)

<u>Beamline</u>	<u>Particle / Energy</u>	<u>flux (/s)</u>	<u>$\langle P \rangle$ (W/ cm)</u>
1. APS	$e^+, e^- / 450 \text{ MeV}$	$5 \cdot 10^{13}$	2
2. IPNS	$p / 450 \text{ MeV}$	$9 \cdot 10^{13}$	5
3. Atlas	heavy nuclei / 100–2000 MeV	low	low
4. LINAC	$e^- / 20 \text{ MeV}$	$3 \cdot 10^{11}$	low

Bates

CEBAF

MSU

SLAC

TRIUMF

Summary & Outlook:

- Have conceptual solutions for main engineering problems
- Plan:
 1. complete finite-element analyses of stresses in graduated windows
 2. continue CFD studies of flow
 3. refine designs & iterate with simulators
 4. refine cost estimates
 5. FY00-01: build and test prototypes
– including high-current beam test
 6. investigate LiH as option
 7. consider high-pressure gaseous hydrogen?